**LA DIFUSIÓN Y CONVECCIÓN BINARIA EN GASES**

**EN UNA CELDA DE DIFUSIÓN-CONVECCIÓN**

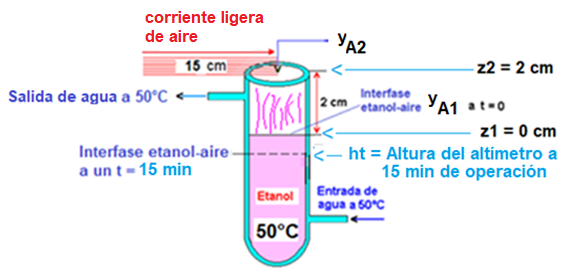
**1.- PROBLEMA**

Utilizar la celda mostrada en la Figura 1 para hacer que se muestre la difusión y también la convección de los vapores de etanol en aire utilizando como medio de contraste humos de incienso y el control manual de la abertura de la válvula que hace pasar aire ambiental por el borde superior de la celda. El propósito de esta experimentación es el de mostrar la diferencia de **las magnitudes iniciales de los fluxes molares NA** por difusión y por convección, ya que en los guiones siguientes del programa de este laboratorio se presentan simultáneamente estos mecanismos.

Calcular el porcentaje que resulta de la relación del flux por difusión al flux por convección al finalizar el tiempo de 15 minutos de operación, ¿Cuál es su opinión sobre el resultado obtenido?

Condiciones de operación de este experimento

* La celda tiene 1.12 cm de diámetro interno.
* Se trabaja con etanol Q.P. a 2 cm abajo del borde de la celda.
* A una temperatura constante de 50°C con una presión de 586 mm Hg que es la presión atmosférica promedio en el laboratorio.



**Figura 1.** La celda de difusión-convección con doble pared de vidrio y con etanol líquido a 2 cm del borde superior de la celda.

**2. PARTE EXPERIEMNTAL**

**2.1** Conectar todos los componentes de este equipo de acuerdo con la **Figura 2.** y recircular agua a 50°C por la doble pared de la celda y alimentar etanol líquido hasta llegar a 2 cm del borde superior.

**NO** accionar el botón de la bomba que proporciona el flujo de aire hasta que la celda de difusión esté llena de humos de incienso. El incienso es el medio que permite ver anticipadamente cuando se logra la difusión o la convección.



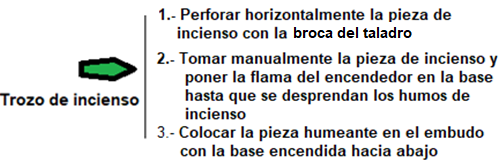
**Figura 2.**  Elementos del equipo para lograr que se manifieste

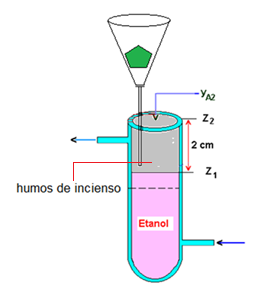
la difusión o la convección.

**2.2** Producción de humos de incienso para que se pueda observar la difusión del etanol en aire.

Después encender un trozo de incienso, colocarlo en el embudo de vidrio como se muestra en la **Figura 3** utilizando el mismo soporte universal donde se encuentra colocada la celda de difusión para llenar de humos el espacio de 2 cm. Una vez que la celda esté llena de humo, retirar el embudo y colocarlo en un vaso Erlenmeyer.

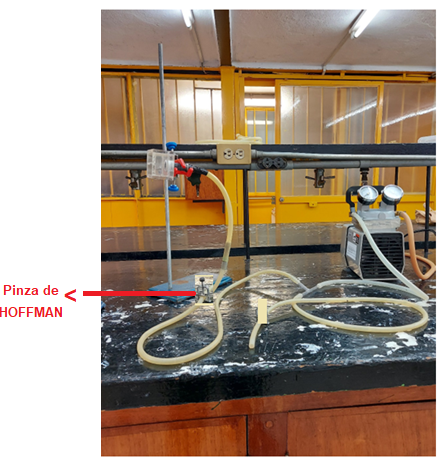
Para encender el trozo de incienso seguir los siguientes pasos:

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**Figura 3.** Alimentación de humos a la celda de difusión

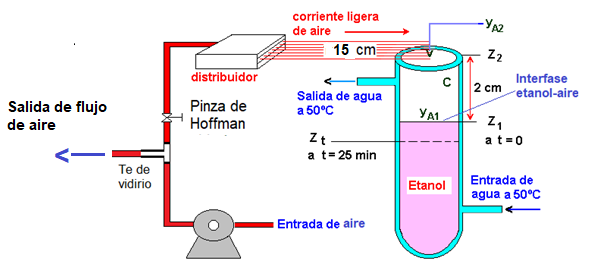
A continuación, asegurarse que la válvula (la pinza de Hoffman o de Mohor) que controla el flujo de aire que circula por el borde superior de la celda esté cerrada y ubicada como lo muestran las **Figura 4.**



**Figura (4).** Observar la ubicación de la pinza de Hoffman para alimentar

la corriente de aire a la celda y lograr que se manifieste la difusión

Medir la distancia de la salida del distribuidor de aire al centro de la celda para que esté aproximadamente a 15 cm, consultar la **Figura 5.**



**Figura (5).** Con una regla de plástico separar la salida del distribuidor de aire y el centro de celda aproximadamente a 15 centímetros para ambos experimentos, el de difusión y el de convección.

Después, abrir LENTAMENTE la pinza de Hoffman para hacer pasar corrientes de aire sobre el borde superior de la celda que contiene humos, se sugiere abrirla observando la celda para que se mantenga una capa estancada de vapores de etanol en aire, como se muestra en la **Figura 6**.

Imagen que contiene interior, taza, cocina, alimentos

Descripción generada automáticamente

**Figura 6**. Los humos de incienso sin remolinos indica la presencia del mecanismo por difusión.

A continuación, retirar los humos de la celda y observar mediante el telescopio del altímetro como el etanol se ha expandido dentro de la celda (ya no está a 2 cm) por lo que es necesario retirar el etanol líquido en exceso con una jeringa ***para que coincidan*** ***la cruz que tiene la lente del altímetro, el menisco del etanol líquido y la marca que fue pintada con un plumón a dos cm del borde superior de la celda.***

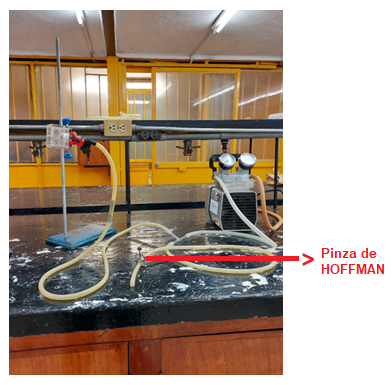
Llenar la **Tabla (1)** con los datos experimentales manteniendo constante la abertura de la pinza de Hoffman.

##### Tabla (1). Datos experimentales para la difusión del etanol en aire

|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- |
| |  |  | | --- | --- | | **Celda**  **Di** **= 1.12 cm**  **A = 0.985 cm2** | | | **t** | **h t** | | (min) | (cm) | | 0 | 0 | | 5 |  | | 10 |  | | 15 |  | | |  |  |  | | --- | --- | --- | | **t**  (min) | **ht**  (cm) | **Lz = Zto** **+ ht** | | 0 | 0 | Zto = 2 | | **15** |  | **Lz = 2 +** |   **ht**= Es la altura que proporciona la pantalla del altímetro a los diferentes tiempos de operación.  **Zto** = Es el eje coordenado de la celda de difusión para un tiempo **to** igual a cero.  **Lz =** Es la longitud del menisco del etanol líquido en la celda a los 15 min de operación |

**2.3** Producción de humos de incienso para que se manifieste la convección del etanol en aire dentro de la celda de vidrio

Para lograrla convección de los vapores de etanol en el aire dentro de la celda de difusión, es necesario seguir el procedimiento anterior pero ahora será necesario cambiar de posición de la celda de Hoffman, así como se muestra en la **Figura 7** abriendo LENTAMENTE la piza de Hoffman para que se formen remolinos convectivos de humos de incienso como los que se muestran en la **Figura 8**.



**Figura 7.** Reubicación de la pinza de Hoffman para lograr

que se muestre la convección

Imagen que contiene interior, tabla, taza, vidrio

Descripción generada automáticamente

**Figura 8.** Operación de la celda de difusión donde se observa la

convección de los humos de incienso mezclado con los

vapores de etanol en aire.

Llenar la **Tabla (2)** con los datos experimentales manteniendo constante la abertura de la pinza de Hoffman cuando se empezó a manifestar la convección.

##### Tabla (2). Datos experimentales para la convección del etanol en aire

|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- |
| |  |  | | --- | --- | | **Celda**  **Di** **= 1.12 cm**  **A = 0.985 cm2** | | | **t** | **h t** | | (min) | (cm) | | 0 | 0 | | 5 |  | | 10 |  | | 15 |  | | |  |  |  | | --- | --- | --- | | **t**  (min) | **ht**  (cm) | **Lz = Zto** **+ ht**  (cm) | | 0 | 0 | Zto = 2 | | **15** |  | **Lz=2 +** |   **ht**= Es la altura que proporciona la pantalla del altímetro a los diferentes tiempos de operación.  **Zto** = Es el eje coordenado de la celda de difusión para un tiempo igual a cero.  **Lz =** Es la longitud del menisco del etanol líquido a 15 min de operación |

**3. MATERIALES**

Un vernier

Un baño de temperatura controlada

Un vaso de precipitados de 600 mL con etanol RA (reactivo analítico)

Un distribuidor de aire con manguera (cajita de acrílico)

Una pinza de Hoffman o una pinza de Mohr

Una te de cristal

Cinco mangueras de hule látex

Cinco celdas de difusión

Un cronómetro

Un catetómetro

Dos soportes universales con pinzas

Un plumón con tinta para escribir en rojo o en negro

Una regla flexible

Una bomba de vacío

Dos jeringas de plástico de 5 mL

Dos embudos de vidrio de talle corto

Dos vasos chicos de Erlenmeyer

Una bolsa con trozos de incienso

Un cúter

Un encendedor

Un taladro con broca

La libreta número 1 de la bitácora del LIQ-III

**3.1 SUSTANCIAS**

600 mL de etanol RA(Reactivo Analítico)

**3.2 SERVICIOS AUXILIARES**

Energía eléctrica de 110 volts

Agua caliente a 50°C

Aire a presión

**4. FOTOGRAFÍA**

![Imagen que contiene tabla, computadora

Descripción generada automáticamente](data:image/jpeg;base64,/9j/4AAQSkZJRgABAQEAAAAAAAD/4RCyRXhpZgAATU0AKgAAAAgAAodpAAQAAAABAAAIMuocAAcAAAgMAAAAJgAAAAAc6gAAAAgAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAFkAMAAgAAABQAABCAkAQAAgAAABQAABCUkpEAAgAAAAMyOQAAkpIAAgAAAAMyOQAA6hwABwAACAwAAAh0AAAAABzqAAAACAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAA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**Figura 9.** Equipo para el estudio de la difusión y la convección

**5. MEDIDAS DE HIGIENE Y SEGURIDAD**

Utilizar lentes de seguridad para el manejo del etanol

**6. DESARROLLO EXPERIMENTAL (incluir arranque, operación y paro)**

Arranque del equipo

**1.-** Dibujar con un plumón una raya roja a 2.0 cm abajo del borde superior de la celda dediámetro interno = 0.95 cm.

**2.-** Utilizar un soporte universal con dos pinzas para sujetar la celda de difusión y el embudo del incienso, conectar la celda al baño de temperatura controlada con mangueras de hule látex.

**3.-** Programar el baño de agua a 50ºC

**4.-** Utilizar otro soporte universal con pinzas para sujetar el distribuidor de aire apuntando la ranura de salida al borde superior de la celda. El distribuidor de aire deberá conectarse con mangueras de hule látex a la bomba de vacío acoplando una manguera de hule, una te de cristal y una pinza de Hoffman para obtener un flujo muy bajo para la difusión y un flujo alto para la convección que fluya perpen-dicular al borde de la celda.

**5.-** Vaciar etanol RA (Reactivo Analítico) a la celda hasta que el menisco del alcohol toque la marca trazada a 2.0 cm de la celda.

**6.-** Hacer coincidir el menisco del etanol contenido en la celda con el puntero óptico de la cruz del catetómetro.

**7.-** Esperar 3 minutos para considerar el factor de expansión del etanol cuando se calienta a 50ºC, después corregir la nueva altura del altímetro, y oprimir el botón de **cero** ubicado en su carátula digital de altímetro.

Operación del equipo

**8.-** Hacer pasar la corriente de aire por la ranura del distribuidor arrancando la bomba de vacío y esperar 30 segundos antes de comenzar el conteo del tiempo con el cronómetro. Durante este tiempo verificar que la ranura del distribuidor de la caja de acrílico esté alineada a la boquilla de la celda y la marca óptica del catetómetro esté alineada con el menisco del etanol, las tres condiciones deben de coinsidir

**9.-** Registrar al final de los tiempos de operación los valores leídos en la carátula del altímetro, después, apuntar nuevamente el puntero óptico a la altura que descendió el etanol

Paro del equipo

**10.-** Apagar los botones de energía eléctrica de la bomba de vacío y del baño de temperatura controlada

**11.-** Apagar el botón de encendido del catetómetro

**12.-** Vaciar el agua caliente del baño de temperatura controlada

**13.-**Desconectar cuidadosamente todas las mangueras de hule látex

1**4.-** Guardar las celdas de difusión-convección en sus bolsas correspondientes

**7. CUESTIONARIO**

**1.-** ¿Cuál es el propósito de hacer pasar una corriente de aire paralela al borde superior de la celda?

**2.-** Si el etanol que se utiliza en la celda de difusión es químicamente puro () utilizar la ley de Dalton-Raoult  para evaluar la fracción mol en la interfase  donde se dan las vaporizaciones del etanol a presión (586 mm Hg) y temperatura (50°C), consultar la expresión para calcular la presión de vapor del etanol (pA°) en el Anexo 12.

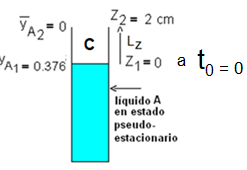
**3.-** Utilizar la información del Apéndice 13 para ver el procedimiento para calcular el coeficiente de difusión binaria DAB = 10.57 cm2/min a presión atmosférica P = 0.771 atm (586 mm Hg) y T = 50°C. NO REPORTAR CÁLCULOS

PM (Etanol) = 46.07 σ (Etanol) = 4.53 A° ε A / K = 362.5

PM (Aire) = 28.97 σ (Aire) = 3.617 A° ε A / K = 97

**4.-** Calcular la concentración de la mezcla gaseosa C dentro de la celda de difusión en gamol de mezcla / cm3 de mezcla.

 ; 



**5.-** Reportar el resultado de la rapidez inicial de vaporización por difusión y la rapidez inicial por convección de los vapores de etanol en aire como fluxes molares en gmol/ min cm2 al finalizar los 15 minutos de operación.

**6.-** Calcular el porcentaje que resulta de la relación del flux por difusión al flux por convección al finalizar el tiempo de 15 minutos de operación, interpretar este resultado

**7.-** Con sus palabras defina que es la difusión molecular y que es la convección molecular

**8. NOMENCLATURA**

***As*** = Área de la superficie interfacial entre el etanol y el aire, área transversal de las celdas de difusión (cm2)

**C** = Concentración de la mezcla gaseosa de la mezcla de los vapores de etanol y aire: gmol de mezcla gaseosa / cm3 de mezcla gaseosa

**DAB** = Coeficiente de difusión binario (cm2 / min)

**ht** = Altura de la base del menisco del etanol en el catetómetro a diferentes tiempos en (cm)

**JAZ** = Rapidez instantánea de transferencia de masa molar por difusión en (gmol EtOH / min cm^2)

**GAZ** = Flujo molar de vaporización del etanol líquido (gmol EtOH / min)

**n** = Exponente adimensional

**P°ETOH**= Presión de vapor del etanol (mm de Hg)

**PMA** = Peso molecular del etanol (g /gmol)

**PT** = Presión total en el Laboratorio de Ingeniería Química = 586 mmHg

**yA** = Fracción mol de etanol en aire

**t** = Tiempo de operación en (min)

**Tc** = Temperatura crítica del etanol en (grados Kelvin)

**TK** = Temperatura de operación en (grados Kelvin)

**W*AZ*** = Flujo de masa molar por difusión y convección del etanol en la fase gaseosa en (gmol EtOH / min)

**Z to** = Altura con valor de 2 cm en la celda de difusión a tiempo cero en (cm)

**Z t** = Altura de los decrementos temporales del nivel del etanol en la celda (cm)

**Z** = Diferencia de alturas entre el borde de las celdas y la altura del menisco del

ETOH (cm)

**t** = Diferencia de tiempo (min)

 = Densidad del etanol en (g / mL)

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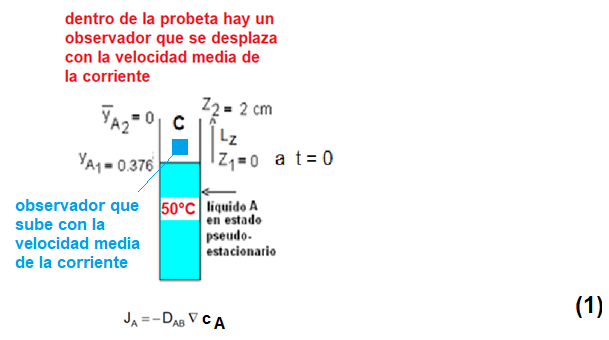
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**10. ANEXOS**

**Anexo 10.1 Difusión molecular**

La ley de difusión de Fick establece que la difusión molecular es proporcional a la disminución del gradiente de concentración; es decir, para una mezcla gaseosa o líquida de dos componentes A y B, el vector densidad de flujo **JA** (o flux por difusión) de la especie A está asociado con respecto a un observador que se desplaza con la velocidad media de la corriente y viene dada por



El flux total **NA** o la densidad de flujo total de la especie A, con respecto a un observador estacionario, es





En estas ecuaciones cA es la concentración del componente A, DAB es la difusividad de A en B (o de B en A), y **yA**es la fracción molar. El segundo término de la ecuación (2) tiene en cuenta el transporte debido al flujo global que está compuesto por el transporte difusional superpuesto al transporte convectivo.

Dos situaciones físicamente frecuentes a las que es aplicable la ecuación (2) son:

**1.-** Contradifusión equimolar donde el número de moles de A que difunden en una dirección es igual al número de moles de B que se difunden en la dirección opuesta; es decir, y la ecuación (2) se reduce a

 (3)

Este caso **NO** se presenta en esta experimentación utilizando la celda de difusión-convección. Cuando se vea en este curso el guion de destilación continua de multicomponentes se analizará con detalle.

**2.-** Difusión unimolecular de un componente A a través de un componente B estancado; es decir . Por lo tanto, la ecuación (2) se reduce a:

 (4)

Que cuando se aplica a través de una película (como es espacio de 2 cm en la celda de difusión-convección) que se extiende desde z1 hasta z2 se transforma en

 (5)

|  |  |
| --- | --- |
|  |  |

**Figura 10. Difusión unimolecular del componente A**

**a través de un componente B estancado**

En la difusión unimolecular el transporte de masa del componente A ocurre a través de un componente B estancado, así NB = 0 y por lo tanto la ecuación (2) se puede aplicar a la altura de la película estancada de coordenada **z**.

 (6)

Integrando desde z1 a cualquier z entre z1 a z2

 (7)

se llega a,

 (8)

De la ecuación (8) se puede despejar **yA**, la variación de la fracción molar en función de la altura de la coordenada z, entre z1 y z2

 (9)

Donde C, es la concentración de la mezcla etanol-aire en gmol de mezcla/cm3 de mezcla y se comporta como mezcla ideal y se calcula con:

, 

Consultar el anexo 10.3 para evaluar el coeficiente de difusión DAB.

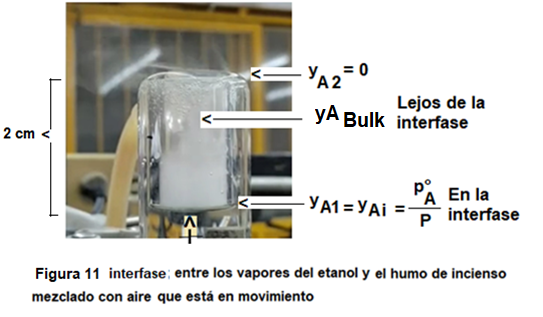
Una alternativa se obtiene cuando la ecuación (7) se integra tomando el valor de

z = z2

 (10)

**10.2 Transferencia de masa en la interfase, el mecanismo por convección**

Para múltiples aplicaciones en ingeniería, es necesario relacionar la rapidez de la transferenciade masa **NAZ**de especies químicas **de una fase a otra**, la cual ocurre a través de una interfase. Una interfase es la superficie frontera entre dos fases que se tocan. En general, las propiedades de cada fase en las regiones de la interfase difieren de las que prevalecen en su seno de cada uno de los filudos lejos de la interface.



La transferencia de masa por convección implica la transferencia de una sustancia a través de una interfase que se forma por el contacto entre fases, y puede ser que alguna de ellas se mueva o ambas se muevan donde la rapidez de transferencia de masa está dada por la siguiente ecuación:

 (11)

Donde el flux de masa, **NA,** ocurre en la dirección de la disminución de la concentración desde **CAi** en la interface a la concentración del seno del fluido **CAb** (b = bulk).

La ecuación (11) se puede aplicar en la altura de la celda dada para la coordenada **z** en los dos centímetros explicados por la Figura 11.

**Aplicación del modelo de la película** [8] **para calcular el coeficiente individual por convección kc**

Se han propuesto varios modelos convectivos **[7]** para describir los fenómenos de transferencia de masa molar que ocurren cuando una fase gaseosa compuesta por dos o más componentes recibe vapores de otra fase líquida que puede contener uno o más compontes y se requiere conocer el flux **NA** de alguno de ellos como buena alternativa se puede aplicar el modelo de la doble película que fue propuesto por Whitman y Lewis.

En la celda de difusión de este experimento se ponen en contacto a través de su interfase etanol puro y aire atmosférico, donde por vaporización se transfiere masa molar al aire y como sólo etanol puro se vaporiza no existe una película del lado del líquido por lo que tampoco del coeficiente individual  como se muestra en la Figura (12).

Para el caso de esta celda de difusión-convección

 (18)

,

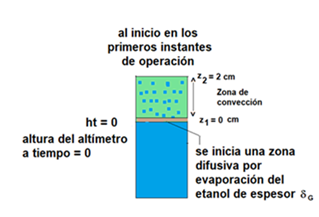
 Es el recorrido del altímetro a un tiempo de 15 minutos

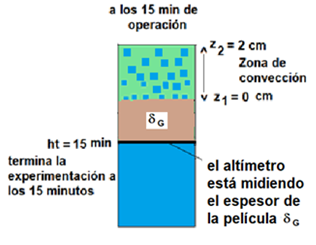
Es importante aclarar que cada equipo de transferencia de masa tiene un coeficiente **kc diferente dependiendo de las variables de su proceso de separación.**

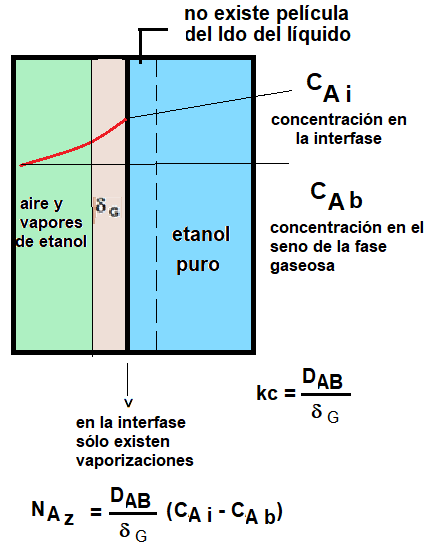
|  |  |
| --- | --- |
| **Fase gaseosa** | |
| NA = kG pA | Moles de A transferidas / (tiempo)(área)(presión) |
| NA = kCCA | Moles de A transferidas / (tiempo)(área)(gmoles/volumen) |
| NA = kyyA | Moles de A transferidas / (tiempo)(área)(fracción mol) |
| NA = kYYA | Moles de A transferidas / (tiempo)(área)(gmol de A / gmol de B) |

|  |  |
| --- | --- |
| **Fase líquida** | |
| NA = kL CA | Moles de A transferidas / (tiempo)(área)(gmol/volumen) **=** longitud/tiempo |
| NA = kxA | Moles de A transferidas / (tiempo)(área)(fracción mol) |
| NA = kyyA | Moles de A transferidas / (tiempo)(área)(fracción mol) |
| NA = kYYA | Moles de A transferidas / (tiempo)(área)(gmol de A / gmol de B) |

A continuación, se muestra el modelo de la película en la celda de difusión-convección considerando sólo la fase gaseosa, el espesor esta película a los 15 minutos de operación es = al valor final del altímetro ht a los 15 minutos – el valor inicial del altímetro ht = 0

****

****

****

**Figura (12).** El modelo de la película para la transferencia de masa molar entre un líquido que se evapora y un gas en una celda de difusión. La transferencia va de la interfase del líquido al aire por vaporizaciones del etanol, no se forma una película del lado del líquido.

**Anexo 10.3 Ecuaciones para calcular densidades, presiones de vapor y el coeficiente de difusión DAB**

**Ecuación para calcular la densidad del etanol (en gramos/cm3**)

A = 0.2657 B = 0.26395

n = 0.23670 Tc = 516.25 °K



**Ecuación para calcular la presión de vapor del etanol en (mm de Hg)**

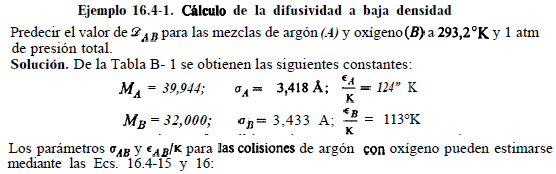
Constantes

A = 23.8442, B = - 2.8642 x 103, C = -5.0474, D = 3.7448 x 10 -11,

E = 2.7361 x 10 - 7



**Información para el cálculo del coeficiente de difusión DAB, consultar la referencia [4], página 16-21.**

****

Texto, Carta

Descripción generada automáticamente

1.003 se calcula con la información de la tabla siguiente B-2

Tabla

Descripción generada automáticamente

Tabla

Descripción generada automáticamente

Para este ejemplo hay que interpolar

|  |  |
| --- | --- |
| kT/eAB  2.30  2.40  2.50  2.60 | 1.026  1.012  0.9996  0.9878 |



Por lo tanto

1.003

